

Quiz 1

Problem 1

A piston-cylinder device contains 0.1 m³ of liquid water and 0.9 m³ of water vapor in equilibrium at 800 kPa. Heat is transferred at constant pressure until the temperature reaches 350°C.

- a) What is the initial temperature of the water?

Initially two phases coexist in equilibrium, thus saturated liquid-vapor mixture. The temperature in the tank must be the saturation temperature at given pressure. From table B1.2, **T_{sat} = 170.43°C**

- b) Determine the total mass of the water.

The total mass in this case can be determined by adding the mass of each phase:

$$m_f = \frac{V_f}{v_f} = \frac{0.1}{0.001115} = 89.704 \text{ kg}$$

$$m_g = \frac{V_g}{v_g} = \frac{0.9}{0.24043} = 3.744 \text{ kg}$$

$$m_T = m_f + m_g = 89.704 + 3.744 = \mathbf{93.447 \text{ kg}}$$

- c) Calculate the final volume.

For the final state, P₂ = 800 kPa and T₂ = 350°C, checking in table B1.2, the water is in the superheated phase. From table B1.3, v₂ = 0.35439 m³/kg

$$V_2 = m_T \times v_2 = 93.447 \times 0.35439 = \mathbf{33.117 \text{ m}^3}$$

- d) Calculate the work done in this process.

The boundary work done in this process is

$$W_{12} = \int_1^2 P dV = P(V_2 - V_1) = 800 \text{ kPa} \times (33.117 - 1) \text{ m}^3 = \mathbf{25694 \text{ kJ}}$$

- e) Find the amount of heat added in kJ:

Take a C.V. Water. This is a control mass.

The cylinder is stationary and thus the kinetic and potential energy changes are negligible.

By applying the 1st law of thermodynamics: $m_T(u_2 - u_1) = Q_{12} - W_{12}$

$$\text{For state 1: } v_1 = \frac{V_1}{m_T} = \frac{1}{93.447} = 0.0107 \text{ m}^3/\text{kg}$$

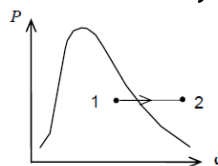
Checking in table B1.2, for P₁ = 800 kPa,

$$x_1 = \frac{v_1 - v_f}{v_g - v_f} = \frac{0.0107 - 0.001115}{0.24043 - 0.001115} = 0.040052$$

$$u_1 = u_f + x_1 u_{fg} = 720.20 + 0.04 \times 1856.58 = 794.57 \text{ kJ/kg}$$

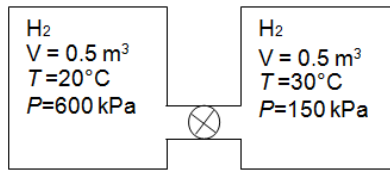
For state 2, Table B1.3, u₂ = 2878.16 kJ/kg

$$Q_{12} = 93.447 \times (2878.16 - 794.57) + 25694 = \mathbf{220399 \text{ kJ.}}$$



Problem 2

A 0.5 m³ rigid tank containing hydrogen at 20°C and 600 kPa is connected by a valve to another 0.5 m³ rigid tank that holds hydrogen at 30°C and 150 kPa. Now the valve is opened and the system is allowed to reach thermal equilibrium with the surroundings, which are at 15°C.



- a) Is it reasonable to assume that in both compartments, hydrogen behaves as ideal gas? Provide the justifications needed.

For hydrogen, critical temperature and pressure can be read from table A.2:

$$P_c = 1.3 \text{ MPa}$$

$$T_c = 33.2 \text{ K}$$

$$\text{For tank A: } P_r = P/P_c = 600/1300 = 0.465$$

$$T_r = T/T_c = 293/33.2 = 8.82$$

Then by referring to graph D1, $Z \approx 1$

$$\text{For tank B: } P_r = 150/1300 = 0.115$$

$$T_r = 303/33.2 = 9.13$$

Then by referring to graph D1, $Z \approx 1$

Hence, in both tanks, H₂ can be considered as an ideal gas.

- b) Determine the final pressure in the tank.

$$\text{The gas constant for hydrogen is } R = \frac{\bar{R}}{M} = \frac{8.314}{2.016} = 4.124 \text{ kJ/kg.K}$$

The total mass is $m = m_A + m_B$

$$m_A = \left(\frac{PV}{RT} \right)_A = \frac{600 \times 0.5}{4.124 \times 293} = 0.248 \text{ kg}$$

$$m_B = \left(\frac{PV}{RT} \right)_B = \frac{150 \times 0.5}{4.124 \times 303} = 0.06 \text{ kg}$$

$$m_T = 0.248 + 0.06 = 0.308 \text{ kg}$$

$$V_T = V_A + V_B = 1 \text{ m}^3$$

$$P_{final} = \frac{mRT_{final}}{V} = \frac{0.308 \times 4.124 \times 288}{1} = \mathbf{365.8 \text{ kPa}}$$

Problem 3

0.5 grams of air are contained within a piston cylinder assembly as shown in the figure below. Initially the piston face is at $x = 0 \text{ m}$, and the spring exerts no force on the piston. As a result of heat transfer, the gas expands raising the piston slowly until it hits the stop. At this point the piston face is located at $x = 0.06 \text{ m}$ and the heat transfer ceases. The piston has a cross sectional area of 0.0078 m^2 and a mass of 10 kg . The spring constant is 9000 N/m . Atmospheric pressure is 1 bar and the acceleration of gravity is $g = 9.81 \text{ m/s}^2$. Friction between the piston and the cylinder wall can be neglected.

- a. Calculate initial pressure of the air;

Initially, the spring exerts no force on the piston. Since there is no friction between the piston and cylinder wall: $\sum F_x = 0$

$$P_{gas} \times A_{piston} = P_{atm} \times A_{piston} + M_{piston}g$$

$$P_{gas} = \mathbf{112.5 \text{ kPa}}$$

- b. Find the work exerted by the air in the lifting process.

As the piston moves from $x=0$ to $x= 0.06\text{m}$, the spring exerts a force on the piston: $F_{spring}=kx$.

The pressure of the gas is then:

$$P_{gas} \times A_{piston} = P_{atm} \times A_{piston} + M_{piston}g + F_{spring}$$

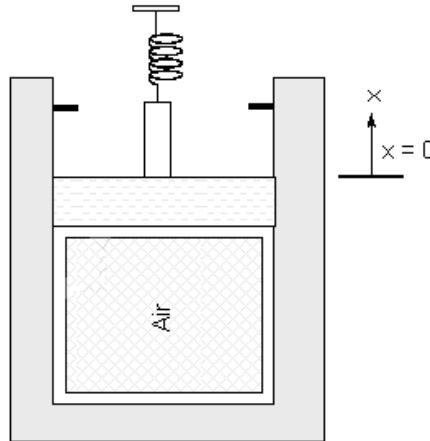
The work done by the gas on the piston is:

$$W = \int_1^2 P_{gas} \times A_{piston} \times dx = \int_{x_1}^{x_2} (P_{atm} \times A_{piston} + M_{piston}g + kx) dx$$

$$W = \left[(P_{atm} \times A_{piston} + M_{piston}g)x + kx^2/2 \right]_0^{0.06}$$

$$W = (10^5 \times 0.078 + 10 \times 9.81)0.06 + 9000 \times (0.06)^2/2$$

$$W = (780 + 98.1)0.06 + 16.2 = \mathbf{68.89 J}$$



Problem 4

A piston-cylinder device contains helium gas initially at 150 kPa, 20°C, and 0.5 m³. The helium is now compressed in a polytropic process ($PV^n = \text{constant}$) to 400 kPa and 140°C.

Assuming that helium behaves as an ideal gas, and considering a constant specific heat at 25°C, calculate the heat loss or gain during this process.

Assumptions

Helium is an ideal gas. From table A2, $M_{\text{HELIUM}} = 4.002 \text{ kg/kmol}$.

$$R = \frac{\bar{R}}{M} = \frac{8.314}{4.002} = 2.077 \frac{\text{kJ}}{\text{kg} \cdot \text{K}}$$

From table A5, for Helium, $C_{v0} = 3.116 \text{ kJ/kg.K}$

The cylinder is stationary and thus the kinetic and potential energy changes are negligible. The 1st law of thermodynamics gives us:

$$m(u_2 - u_1) = Q_{12} - W_{12}$$

The mass and work must be determined.

$$m = \frac{P_1 V_1}{RT_1} = \frac{150 \times 0.5}{2.077 \times 293} = 0.123 \text{ kg}$$

To find the work, n must be found:

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$

and $V_2 = 0.264 \text{ m}^3$

On the other hand, polytropic process: $P_1 V_1^n = P_2 V_2^n$ then

$$\frac{P_1}{P_2} = \left(\frac{V_2}{V_1} \right)^n \Rightarrow n = 1.536$$

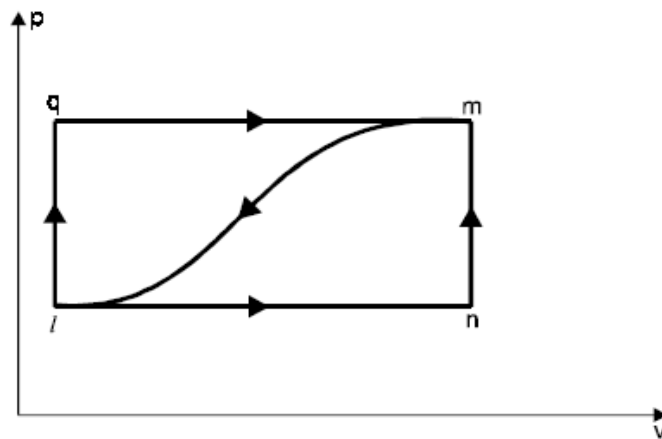
$$W = \frac{P_2 V_2 - P_1 V_1}{1 - n} = \frac{mR(T_2 - T_1)}{1 - n} = \frac{0.123 \times (413 - 293)}{-0.536} = -57.2 \text{ kJ}$$

$$Q_{12} = m(u_2 - u_1) + W_{12} = mC_{v0}(T_2 - T_1) + W_{12} = 0.123 \times 3.116(413 - 293) - 57.2 = \mathbf{-11.2 kJ}$$

Problem 5

When a system is taken from state l to state m , in the figure below, along the path lqm , 168 kJ of heat flows into the system, and the system does 64 kJ of work:

- How much will be the heat that flows into the system along path lnm if the work done is 21 kJ?
- When the system is returned from m to l along the curved path, the work done on the system is 42 kJ. Does the system absorb or liberate heat, and how much of the heat is absorbed or liberated?
- If $U_l = 0$ and $U_n = 84$ kJ, find the heat absorbed in the processes ln and nm .



$$Q_{l-q-m} = 168 \text{ kJ and } W_{l-q-m} = 64 \text{ kJ}$$

We have

$$Q_{l-q-m} = (U_m - U_l) + W_{l-q-m}$$

$$168 = (U_m - U_l) + 64$$

\therefore

$$(U_m - U_l) = 104 \text{ kJ}$$

(a)

$$Q_{l-n-m} = (U_m - U_l) + W_{l-n-m} \\ = 104 + 21 = \mathbf{125 \text{ kJ.}}$$

(b)

$$Q_{m-l} = (U_m - U_l) + W_{m-l} \\ = -104 + (-42) = \mathbf{-146 \text{ kJ.}}$$

The system liberates 146 kJ.

(c)

$$W_{l-n-m} = W_{l-n} + W_{n-m} = W_{l-m} = 21 \text{ kJ} \\ [W_{n-m} = 0, \text{ since volume does not change.}]$$

\therefore

$$Q_{l-n} = (U_n - U_l) + W_{l-n} \\ = (84 - 0) + 21 = \mathbf{105 \text{ kJ.}}$$

Now

$$Q_{l-m-n} = 125 \text{ kJ} = Q_{l-n} + Q_{n-m}$$

\therefore

$$Q_{n-m} = 125 - Q_{l-n} \\ = 125 - 105 = \mathbf{20 \text{ kJ.}}$$

Bonus Problem

A student living in a 4-m X 6m X 6m dormitory room turns on his/her 150-W fan before he/she leaves the room on a summer day, hoping that the room will be cooler when he/she comes back in the evening. Assuming all the doors and windows are tightly closed and disregarding any heat transfer through the walls and the windows, determine the temperature in the room when he/she comes back 10 hours later. Use specific heat values at room temperature, and assume the room to be at 100 kPa and 15°C in the morning when he/she leaves.

Assumptions:

Air is an ideal gas since it is at a high temperature and low pressure relative to its critical point values

The kinetic and potential energy changes are negligible,

Constant specific heats at room temperature can be used for air.

All the doors and windows are tightly closed, and heat transfer through the walls and the windows is disregarded.

The following properties are needed from Table A-5:

The molecular mass of air = 28.97

The specific heat capacity for air at constant volume and room temperature $c_v = 0.717$ kJ/kg.K

We take the room as the system. This is a *closed system* since the doors and the windows are said to be tightly closed, and thus no mass crosses the system boundary during the process. The energy balance for this system can be expressed as:

$$\begin{aligned} W_{e,in} &= \Delta U \\ W_{e,in} &= m(u_2 - u_1) \cong mc_v(T_2 - T_1) \end{aligned} \quad (1)$$

The volume of air in the room = $4 \times 6 \times 6 = 144$ m³

The mass of the air in the room

$$m = \frac{P_1 V}{R^* T_1} = \frac{100 \times 144}{\left(\frac{8.314}{28.97}\right) \times 288} = 174.2 \text{ kg}$$

The electrical work done by the fan = $W_{e,in} = \dot{W}_{e,in} \Delta t = 0.15 \times 10 \times 3600 = 5,400$ kJ

Substituting into equation above and using c_v value at room temperature:

$$5,400 = 174.2 \times 0.717 \times (T_2 - 288)$$

$$\therefore T_2 = 331.2 \text{ K} = \mathbf{58.2^\circ\text{C}}$$