

## Chemistry 217

### Problem Set 6 Solutions

6.1 10 mol of H<sub>2</sub> and 2 mol O<sub>2</sub> at 298 K and 1 bar

$$\Delta S^\circ = -R(n_1 \ln Y_1 + n_2 \ln Y_2)$$

$$Y_1 = \frac{n_1}{n_1 + n_2}, \quad Y_2 = \frac{n_2}{n_1 + n_2}$$

$$\Delta S^\circ = -8.314 \text{ J.K}^{-1} \cdot \text{mol}^{-1} \left( 10 \text{ mol} \times \ln \frac{10}{12} + 2 \text{ mol} \times \ln \frac{2}{12} \right) = 44.95 \text{ J.K}^{-1}$$

6.2 (a)  $S = n_A \bar{S}_A + n_B \bar{S}_B + n_C \bar{S}_C$

$$= n_A \bar{S}_A^\circ + n_B \bar{S}_B^\circ + n_C \bar{S}_C^\circ - R(n_A \ln Y_A + n_B \ln Y_B + n_C \ln Y_C) - \left( (n_A + n_B + n_C) R \ln \left( \frac{P}{P^\circ} \right) \right)$$

(b)  $S = [n_A \bar{S}_A + n_B \bar{S}_B] + n_C \bar{S}_C$

$$= \left[ n_A \bar{S}_A^\circ + n_C \bar{S}_C^\circ - R(n_A \ln Y_A + n_C \ln Y_C) - \left( (n_A + n_C) R \ln \left( \frac{P_I}{P^\circ} \right) \right) \right] + n_B \bar{S}_B$$

$$= n_I \left[ r_A \bar{S}_A^\circ + r_C \bar{S}_C^\circ - R(r_A \ln r_A + r_C \ln r_C) - \left( R \ln \left( \frac{P_I}{P^\circ} \right) \right) \right] + n_B \bar{S}_B$$

$$n_I = n_A + n_C, \quad P_I = P_A + P_C$$

(c)  $S = n_I \bar{S}_I + n_B \bar{S}_B = n_I [Y_I \bar{S}_I + Y_B \bar{S}_B]$

$$= n_I \left[ Y_I \bar{S}_I^\circ - Y_I R \ln \left( \frac{P_I}{P^\circ} \right) + Y_B \bar{S}_B^\circ - Y_B R \ln \left( \frac{P_B}{P^\circ} \right) \right]$$

$$= n_I \left[ Y_I \bar{S}_I^\circ + Y_B \bar{S}_B^\circ - R(Y_I \ln Y_I + Y_B \ln Y_B) - R \ln \left( \frac{P}{P^\circ} \right) \right]$$

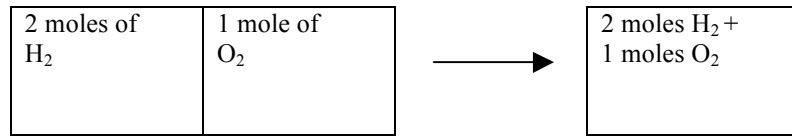
Rearranging the above equation can lead to equation (a)

6.3

(a)  $\Delta G_{\text{mix}} = RT(y_1 \ln y_1 + y_2 \ln y_2)$   
 $= (8.314 \text{ J.K}^{-1} \cdot \text{mol}^{-1})(298.15 \text{ K})(0.8 \ln 0.8 + 0.2 \ln 0.2) = -1239 \text{ J.mol}^{-1}$

$$\Delta S_{\text{mix}} = -R(y_1 \ln y_1 + y_2 \ln y_2) = 4.159 \text{ J.K}^{-1} \cdot \text{mol}^{-1}$$

(b) 25°C, 1.00 bar



$$\Delta H_{\text{H}_2} = 0$$

$$\begin{aligned} \text{H}_2: \Delta S_{\text{mix}} &= \int \frac{dq_{\text{rev}}}{T} = -\int \frac{dw}{T} = \int \frac{PdV}{T} = \int \frac{nR}{V} dV = nR \ln \frac{V_f}{V_i} \\ &= (2 \text{ mol})(8.314 \text{ J.K}^{-1} \cdot \text{mol}^{-1}) \ln \left( \frac{3}{2} \right) = 6.74 \text{ J.K}^{-1} \end{aligned}$$

$$\Delta H_{\text{O}_2} = 0$$

$$\text{O}_2: \Delta S_{\text{mix}} = 1 \times (8.314) \ln \left( \frac{3}{1} \right) = 9.13 \text{ J.K}^{-1}$$

$$\Delta S_{\text{mix}} = \Delta S_{\text{mix, H}_2} + \Delta S_{\text{mix, O}_2} = 15.9 \text{ J.K}^{-1}$$

$$\Delta G_{\text{mix}} = \Delta H_{\text{mix}} - T\Delta S_{\text{mix}} = 0 - 298.15 \text{ K} \times 15.9 \text{ J.K}^{-1} = -4740 \text{ J}$$

#### 6.4. EU & Al-Ghoul, Chapter 7

Problem 1 :

$$V = 1.00294 + 0.0194m + 0.00214m^{3/2} + 2.7 \times 10^{-6} m^{5/2}$$

$$\bar{V}_{\text{NaCl}} = \left( \frac{\partial V}{\partial m_{\text{NaCl}}} \right)_{T, P, n_{\text{water}}} = 0.0164 + 0.00321m^{1/2} + 6.75 \times 10^{-6} m^{3/2} \text{ (L)}$$

$$\bar{V}_{\text{water}} = -\frac{n_{\text{NaCl}} \bar{V}_{\text{NaCl}}}{n_{\text{water}}} = -\frac{n_{\text{NaCl}} M_{\text{water}} \bar{V}_{\text{NaCl}}}{m_{\text{water}}}$$

$$= -m \times M_{\text{water}} \times 10^{-3} \times \bar{V}_{\text{NaCl}} = -0.018m \times \bar{V}_{\text{NaCl}}$$

$$\Rightarrow \bar{V}_{\text{water}} = -2.952 \times 10^{-4} m - 5.778 \times 10^{-5} m^{3/2} - 1.215 \times 10^{-7} m^{5/2} \text{ (L)}$$

Problem 2 :

$$V_{\text{Total}} = n_{\text{water}} \bar{V}_{\text{water}} + n_{\text{ethanol}} \bar{V}_{\text{ethanol}}$$

$$\Rightarrow \bar{V}_{\text{ethanol}} = \frac{V_{\text{Total}} - n_{\text{water}} \bar{V}_{\text{water}}}{n_{\text{ethanol}}} = \frac{0.06816 - 1.158 \times 0.01698}{0.842} = 0.057 \text{ L.mol}^{-1}$$

Problem 3 :

$$V_{m_{H_2O}} = \frac{M_{H_2O}}{d_{H_2O}} = \frac{1.802 \times 10^{-2}}{0.997} = 1.81 \times 10^{-2} \text{ L.mol}^{-1}$$

$$\frac{V_{m_{H_2O}}}{\bar{V}_{H_2O}} = \frac{1.81 \times 10^{-2}}{1.70 \times 10^{-2}} = 1.06$$

$$V_{m_{ethanol}} = \frac{M_{ethanol}}{d_{ethanol}} = \frac{4.602 \times 10^{-2}}{0.7852} = 5.861 \times 10^{-2} \text{ L.mol}^{-1}$$

$$\frac{V_{m_{ethanol}}}{\bar{V}_{ethanol}} = \frac{5.86 \times 10^{-2}}{5.7 \times 10^{-2}} = 1.03$$

**Problem 4 :**

According to the Gibbs—Duhem equation for a single component:

$$SdT - VdP = -nd\mu$$

$$\Rightarrow S = V \left( \frac{\partial P}{\partial T} \right)_V - n \left( \frac{\partial \mu}{\partial T} \right)_V$$

$$\left( \frac{\partial S}{\partial T} \right)_V = V \left( \frac{\partial^2 P}{\partial T^2} \right)_V - n \left( \frac{\partial^2 \mu}{\partial T^2} \right)_V$$

$$C_V = T \left( \frac{\partial S}{\partial T} \right)_V \Rightarrow \frac{C_V}{T} = \left( \frac{\partial S}{\partial T} \right)_V$$

$$\frac{C_V}{T} = V \left( \frac{\partial^2 P}{\partial T^2} \right)_V - n \left( \frac{\partial^2 \mu}{\partial T^2} \right)_V \Rightarrow \frac{C_V}{V} = T \left[ \left( \frac{\partial^2 P}{\partial T^2} \right)_V - \frac{n}{V} \left( \frac{\partial^2 \mu}{\partial T^2} \right)_V \right]$$

$$\Rightarrow C_V = T \left[ \left( \frac{\partial^2 P}{\partial T^2} \right)_V - n \left( \frac{\partial^2 \mu}{\partial T^2} \right)_V \right]$$

**6.5** Plot  $\ln(P/KPa)$  vs.  $1000/T$

$$(a) \text{ slope} = -2.34 \times 10^3 \text{ K} = \frac{\Delta H_{\text{vap}}}{(2.303)(8.314 \text{ J.K}^{-1}.\text{mol}^{-1})}$$

$$\Delta H_{\text{vap}} = 44.8 \text{ kJ.mol}^{-1}$$

$$(b) \ln\left(\frac{12.3}{100}\right) = \frac{44800}{8.3145} \left( \frac{1}{T} - \frac{1}{373.15} \right)$$

$$T = \frac{1}{\left( \frac{83145}{44800} \right) \ln\left(\frac{112.3}{100}\right) + \left( \frac{1}{373.15} \right)} = 370.18 \text{ K} = 97.03^\circ \text{C}$$

**6.6** For  $C_{10}H_8$ ,  $P_{\text{vap}}(359\text{K}) = 1.3 \times 10^{-2} \text{ bar}$   
 $P_{\text{vap}}(392\text{K}) = 5.3 \times 10^{-2} \text{ bar}$

(a) Using the Clausius-Clapeyron equation (6.14 in S&A)

$$\ln\left(\frac{P_2}{P_1}\right) = \frac{\Delta\bar{H}_{\text{vap}}(T_2 - T_1)}{RT_1T_2}$$

$$\Delta\bar{H}_{\text{vap}} = \frac{RT_1T_2}{T_2 - T_1} \ln\left(\frac{P_2}{P_1}\right) = \frac{8.314\text{J.K}^{-1}.\text{mol}^{-1}(359\text{K})(392\text{K})}{392\text{K} - 359\text{K}} \ln\left(\frac{5.3 \times 10^{-2}\text{bar}}{1.3 \times 10^{-2}\text{bar}}\right) = 50\text{kJ}.\text{mol}^{-1}$$

Use the Clausius-Clapeyron again but

$$P_{\text{vap}}(T_b) = 1\text{atm} = 1.013\text{bar} = \frac{49900\text{kJ}.\text{mol}^{-1}(T_b - 359\text{K})}{8.314\text{J}.\text{K}^{-1}.\text{mol}^{-1}T_b 359\text{K}}$$

$$\frac{T_b - 359\text{K}}{T_b} = 0.26053$$

$$T_b = \frac{358.95\text{K}}{1 - 0.26053} = 485\text{K}$$

$$\Delta\bar{S}_{\text{vap}} = \frac{\Delta\bar{H}_{\text{vap}}}{T_b} = \frac{49.9\text{kJ}.\text{mol}^{-1}}{485\text{K}} = 102.9\text{J}.\text{K}^{-1}.\text{mol}^{-1}$$

(b) At the triple point,  $T_t = 353.65\text{K}$

$$\ln\frac{P_t}{1.3 \times 10^{-2}\text{bar}} = \frac{\Delta\bar{H}_{\text{vap}}(T_t - 359\text{K})}{T_t - 359\text{K}} = \frac{50000\text{J}.\text{mol}^{-1}(-5.35\text{K})}{8.315\text{J}.\text{K}^{-1}.\text{mol}^{-1}(353.65\text{K} - 359\text{K})} = -0.25233$$

$$P_t = 1.3 \times 10^{-2}\text{bar} \cdot e^{-0.25233} = 0.01010\text{bar} = 0.0101\text{bar}$$

(c)  $P_{\text{sub}} = 1.3 \times 10^{-3}\text{bar}$  @  $T_{\text{sub}} = 325.7\text{K}$

$P_t = 0.0101\text{bar}$  @  $T_t = 353.65\text{K}$

$$\ln\left(\frac{P_{\text{sub}}}{P_t}\right) = \frac{\Delta\bar{H}_{\text{sub}}}{R} \left(\frac{T_{\text{sub}} - T_t}{T_{\text{sub}}T_t}\right)$$

$$\Delta\bar{H}_{\text{sub}} = R \left(\frac{T_{\text{sub}}T_t}{T_{\text{sub}} - T_t}\right) \ln\left(\frac{P_{\text{sub}}}{P_t}\right) = (8.314\text{J}.\text{K}^{-1}.\text{mol}^{-1}) \left(\frac{325.7\text{K} \times 353.65\text{K}}{325.7\text{K} - 353.65\text{K}}\right) \ln\left(\frac{1.3 \times 10^{-3}}{0.0101}\right) = 70\text{kJ}.\text{mol}^{-1}$$

$$\Delta\bar{H}_{\text{fus}} + \Delta\bar{H}_{\text{vap}} = \Delta\bar{H}_{\text{sub}}$$

$$\Delta\bar{H}_{\text{fus}} = \Delta\bar{H}_{\text{sub}} - \Delta\bar{H}_{\text{vap}}$$

$$\Delta\bar{H}_{\text{fus}} = 20\text{kJ}.\text{mol}^{-1}$$

(d)  $P_{\text{C}_{10}\text{H}_8}(\text{s}) = 1.00\text{g}.\text{cm}^{-3}$ ,  $P_{\text{C}_{10}\text{H}_8}(\text{l}) = 0.98\text{g}.\text{cm}^{-3}$

Clapeyron equation

$$\frac{dP}{dT} = \frac{\Delta \bar{H}_{\text{fus}}}{T \Delta \bar{V}}$$

$$\int_{P_1}^{P_2} dP = \frac{\Delta \bar{H}_{\text{fus}}}{\Delta \bar{V}} \int_{T_1}^{T_2} \frac{dT}{T}$$

$$\Delta P = \frac{\Delta \bar{H}_{\text{fus}}}{\Delta \bar{V}} \ln \left( \frac{T_2}{T_1} \right)$$

$$T_2 = T_1 e^{\frac{\Delta P \Delta \bar{V}}{\Delta \bar{H}_{\text{fus}}}}$$

$$\frac{dP}{dT} = \frac{\Delta \bar{H}_{\text{fus}}}{T} \left( \frac{1}{\frac{m}{P(l)} - \frac{m}{P(s)}} \right) = \frac{\Delta \bar{H}_{\text{fus}}}{T} \left( \frac{m}{0.0204 \text{g} \cdot \text{cm}^{-3}} \right)$$

$$\text{so } \frac{dP}{dT} > 0 \Rightarrow \frac{\Delta P}{\Delta T} > 0 \text{ and } \Delta P > 0$$

$$\Delta T > 0 \text{ or } T > 80.5^\circ\text{C}$$

6.7 (a) Find  $T_2$

$$\ln \left( \frac{P_2}{P_1} \right) = \frac{\Delta H}{R} \left( \frac{T_2 - T_1}{T_2 T_1} \right)$$

$$\Delta H_{\text{vap}} = 92 \text{J} \cdot \text{mol}^{-1}, T_1 = 2\text{K}, P_1 = 0.032 \text{bar}, P_2 = 10^{-3} \text{bar}$$

$$\ln \left( \frac{10^{-3} \text{bar}}{0.032 \text{bar}} \right) = \frac{92 \text{J} \cdot \text{mol}^{-1}}{8.314 \text{J} \cdot \text{K}^{-1} \cdot \text{mol}^{-1}} \left( \frac{T_2 - 2}{2T_2} \right)$$

$$-0.3132 = \frac{T_2 - 2}{2T_2}$$

$$T_2 = 1.23 \text{K}$$

(b)  $4 \text{J} \cdot \text{min}^{-1}$ ,  $\Delta H_{\text{vap}} = 92 \text{J} \cdot \text{mol}^{-1}$

$$\frac{4}{92} = 0.04 \text{mol} \cdot \text{min}^{-1} \text{He(g)}$$

Use ideal gas eq'n:  $PV = nRT$ ;  $V = nRT/P$

$$V = \frac{(0.04 \text{ mol} \cdot \text{min}^{-1})(0.08314 \text{ L} \cdot \text{bar} \cdot \text{K}^{-1} \cdot \text{mol}^{-1})(300 \text{ K})}{10^{-3} \text{ bar}} = 997.68 \text{ L} \cdot \text{min}^{-1}$$

- 6.8 (a) Sarin: Vapor pressure = 0.00387 bar at 298K

The boiling point at 1 bar is 158°C = 431.15K

$$\Delta H_{\text{vap}} = \frac{RT_1T_2}{(T_2 - T_1)} \ln\left(\frac{P_2}{P_1}\right) = \frac{(8.314)(298\text{K})(431.15\text{K})}{(133.15\text{K})} \ln\left(\frac{1.01325\text{bar}}{0.00387\text{bar}}\right) = 44666 \text{ J} \cdot \text{mol}^{-1}$$

VX: Vapor pressure =  $9.33 \times 10^{-7}$  bar at 298K

Boiling point at 1 bar is 298°C = 571.15K

$$\Delta H_{\text{vap}} = \frac{(8.314)(298\text{K})(571.15\text{K})}{(273.15\text{K})} \ln\left(\frac{1.01325\text{bar}}{9.33 \times 10^{-7} \text{ bar}}\right) = 71999 \text{ J} \cdot \text{mol}^{-1}$$

- (b) Test Trouton's Rule

$$\text{Sarin: } \Delta S_{\text{vap}} = \frac{\Delta H_{\text{vap}}}{T_b}$$

$$\Delta S_{\text{vap}} = \frac{44666 \text{ J} \cdot \text{mol}^{-1}}{431.15 \text{ K}} = 103.599 \text{ J} \cdot \text{K}^{-1} \cdot \text{mol}^{-1}$$

$$\text{VX: } \Delta S_{\text{vap}} = \frac{71999 \text{ J} \cdot \text{mol}^{-1}}{571.15 \text{ K}} = 126.0597 \text{ J} \cdot \text{K}^{-1} \cdot \text{mol}^{-1}$$

- (c) Change the unit for mg/m<sup>3</sup> to g/l

$$3 \times 10^{-6} \text{ mg} \cdot \text{m}^{-3} = 3 \times 10^{-9} \text{ mg} \cdot \text{l}^{-1} = 3 \times 10^{-12} \text{ g} \cdot \text{l}^{-1}$$

$$\text{For Sarin: } 2 \times 10^{-14} \text{ mol} \cdot \text{l}^{-1}$$

$$\frac{n}{V} = 2 \times 10^{-14} \text{ mol.l}^{-1}$$

$$\frac{P}{RT} = \frac{n}{V}$$

$$P = (2 \times 10^{-14} \text{ mol.l}^{-1})(8.314)(431.15\text{K}) = 7.17 \times 10^{-11} \text{ bar}$$

then use :

$$\ln\left(\frac{P_2}{P_1}\right) = \frac{\Delta H_{\text{vap}}}{R} \left(\frac{T_2 - T_1}{T_2 T_1}\right) \text{ to find } T_1, T_2 = 298\text{K}, P_2 = 0.00387\text{bar}$$

$$\ln\left(\frac{0.00387\text{bar}}{7.17 \times 10^{-11} \text{ bar}}\right) = \frac{44666\text{J.mol}^{-1}}{8.314} \left(\frac{298 - T_1}{298 T_1}\right)$$

$$0.003313 = \frac{298 - T_1}{298 T_1}$$

$$0.9875 T_1 = 298 - T_1 \Rightarrow T_1 = 149.93\text{K}$$

For VX:  $1 \times 10^{-14} \text{ mol.l}^{-1}$

$$\text{VX: } \frac{n}{V} = 1 \times 10^{-14} \text{ mol.l}^{-1}$$

$$\frac{P}{RT} = \frac{n}{V}, P = 4.749 \times 10^{-11} \text{ bar}$$

$$\ln\left(\frac{9.33 \times 10^{-7} \text{ bar}}{4.749 \times 10^{-11} \text{ bar}}\right) = \frac{71999\text{J.mol}^{-1}}{8.314} \left(\frac{298 - T_1}{298 T_1}\right) \Rightarrow T_1 = 222.36\text{K}$$