

Key Solution

CHEN 490 – Fundamentals of Petroleum Engineering
HW #6– Due 10/12/2013

Pressure Drop Problem

To illustrate the pressure loss calculations for each system component, let us work the following complete example. As stated in the equation

$$\Delta P_t = \Delta P_s + \Delta P_p + \Delta P_c + \Delta P_b + \Delta P_{ac} + \Delta P_{ap}$$

Where ΔP_t = pump discharge pressure

ΔP_s = Pressure loss in surface stand pipe, piping, and mud hose

ΔP_p = Pressure loss in drill pipe

ΔP_c = Pressure loss inside drill collars

ΔP_b = Pressure loss across nozzles

ΔP_{ac} = Pressure loss in annulus around collars

ΔP_{ap} = Pressure loss in annulus around drill pipe

Operating Data

Depth = 6000 ft (5500 ft drill pipe, 500 ft drill collars)

Drill pipe = 4 ½ in. internal flush, 16.6 lb/ft (i. d. = 3.826 in)

Drill collars = 6 ¾ in (i. d. = 2.813 in)

Mud density = 10 lb/gal

μ_p = 30 cp

Y_b = 10 lb/100ft²

Bit = 7 7/8 in 3 cone, jet rock bit

Nozzle velocity = at least 25 ft/sec per in of bit diameter (this value is obtained by a commonly applied rule of thumb).

What hydraulic (pump output) horse power will be required for these conditions?

Assumptions:

Circulation rate: This is a fast drilling, soft rock area and that 180 ft/min (3 ft/sec) upward velocity based on a gauge hole is required.

Q = annulus area X velocity, nozzle size is 13/32 in. This nozzle allows an actual velocity V_{act} ,

$$V_{act} = (q/3)/(2.45d^2)$$

Surface equipment losses (standpipe, swivel, Kelly joint, and the piping between the pump and stand pipe). Since this part of the system causes only a small fraction of the total losses, it will be satisfactory to choose an approximate the actual case. Assume $\Delta P_s = 27$ psi

For pressure drop inside drill pipe, calculate the critical velocity.

Pressure drop across bit. This is a jet bit with a nozzle coefficient of 90%.

Calculation Steps:

1. This is obtained from the desired annular velocity necessary for proper hole cleaning (cutting removal). As given, this is a fast drilling, soft rock and that 180 ft/min (3 ft/sec) upward velocity.

2. The flow rate q is in gal/min

$$\begin{aligned} q &= (\text{annulus area})(\text{velocity}) \\ &= 2.45(d_h^2 - d_p^2)v \\ &= 2.45(62 - 20.25)(3) \\ &= 308 \text{ gal/min} \end{aligned}$$

3. Nozzle Size:

3 nozzles (one for each cone) will be used, hence $\frac{1}{3}q$ will flow through each.

For $v = 250$ ft/sec thru each

$$v = \frac{q}{A} = \frac{\frac{1}{3}q}{A}$$

Common field units:

$$v = \frac{\text{ft}}{\text{sec}}$$

$$q = \text{gal/min}$$

$$A = \frac{\pi}{4}d^2 = (.7854)d^2, d = \text{in}$$

Then,

$$v = \frac{q}{(.7854)d^2}$$

where q in gal/min must be equivalent to $\frac{\text{ft}^3}{\text{sec}}$ and d must be equivalent to d in feet in order for v to be in ft/sec

$$\text{then, } \frac{\text{ft}}{\text{sec}} = \frac{\frac{\text{gal}}{7.48 \text{ gal/ft}^3} \times \frac{1}{\text{min}(60 \text{ sec/min})}}{(.7854) \left(\frac{\text{in}}{12}\right)^2}$$

$$\text{where } \frac{\text{gal}}{7.48} = \text{ft}^3$$

$$\text{Min}(60) = \text{sec}$$

$$\left(\frac{12}{12}\right)^2 = \text{ft}^2$$

or

$$\frac{\text{ft}}{\text{sec}} = \frac{\text{gal/min}}{(7.854)(60)} \times \frac{144}{(.7854)(\text{in}^2)} = 0.4085 \frac{\text{gal/min}}{\text{in}^2}$$

In Common form,

$$\frac{\text{ft}}{\text{sec}} = \frac{1}{2.45} \frac{\text{gal/min}}{\text{in}^2}$$

or

$$v = \frac{q}{2.45 d^2}, \quad \text{where } v = \frac{\text{ft}}{\text{sec}}$$

$$q = \frac{\text{gal}}{\text{min}}$$

$$d = \text{in}$$

then,

$$(2.45)(v)(d^2) = q$$

$$d = \sqrt{\frac{q}{2.45 v}} = \sqrt{\frac{\frac{1}{3} q}{2.45 v}}$$

$$= \sqrt{\frac{308}{3(2.45)(250)}}$$

$$d = 0.41 \text{ in}$$

The nearest stock nozzle is $\frac{13}{32}$ in (given)

$$v = \frac{103}{(2.45) \left(\frac{13}{32}\right)^2}$$

$$\approx 225 \text{ ft/sec}$$

4. Surface equipment losses: The surface equipment consists of the standpipe, swivel, Kelly joint, and the piping between the pump and standpipe. Since this part of the system causes only a small fraction of the total losses, it will be satisfactory to choose the one assumed which closely approximates the actual case ($q = 308 \rightarrow \Delta p \cong 30 \text{ psi}$) - then assume $\Delta P_s \cong 27 \text{ psi}$

5. Pressure drop inside drill pipe:

The critical velocity is calculated using the eqn.

$$\begin{aligned}
 V_c &= \frac{1.08 \mu_p + 1.08 \sqrt{\mu_p^2 + 9.3 C_m d^2 \gamma_b}}{\rho_m d} \\
 &= \frac{(1.08)(30) + 1.08 \sqrt{(30)^2 + (9.3)(10)(3.826)^2(10)}}{(10)(3.826)} \\
 &= 4.2 \text{ ft/sec}
 \end{aligned}$$

The V_{act} inside drill pipe is:

$$V_{act} = \frac{q}{(2.45)(d^2)} = \frac{308}{(2.45)(3.826)^2} = 8.58 \text{ ft/sec}$$

Since $8.58 > 4.2$, flow is turbulent and the equation

$$\begin{aligned}
 \text{(equivalent)}, NRe &= \frac{2970 \rho V_{act} d}{\mu_p} \\
 &= \frac{(2970)(10)(8.58)(3.826)}{30} \\
 &= 32,500
 \end{aligned}$$

From chart, Fanning friction factor f vs NRe , Curve II

$$f \cong 0.0066$$

For turbulent flow, Use Fanning equation

$$\begin{aligned}\Delta P_f &= \frac{f_e L v^2}{25.8 d} \\ &= \frac{(0.0066)(10)(5500)(8.58)^2}{(25.8)(3.826)} \\ &= 270 \text{ psi}\end{aligned}$$

6. Pressure drop inside chill collar:

$$v_{act} = \frac{308}{(2.45)(2.813)^2} = 15.9 \text{ ft/sec}$$

∴, flow is turbulent, by inspection

$$\begin{aligned}NR_e &= \frac{(2970)(10)(15.9)(2.813)}{30} \\ &= 44300\end{aligned}$$

$$f \approx 0.0062$$

$$\begin{aligned}\Delta P_{fc} &= \frac{(0.0062)(10)(500)(15.9)^2}{(25.8)(2.813)} \\ &= 108 \text{ psi}\end{aligned}$$

7. Pressure drop across bit:

This is a jet bit with a nozzle coefficient of 0.95, ∴, equation $d_e = \sqrt{nd^2}$ corrected for multiple nozzles, is used

$$d = \sqrt{(3)\left(\frac{13}{32}\right)^2} = 0.704 \text{ in}$$

$$\begin{aligned}\Delta P_{fb} &= \frac{q^2 \rho_m}{7430 c^2 d^4} \\ &= \frac{(308)^2 (10)}{(7430)(0.95)^2 (0.704)^2} = 580 \text{ psi}\end{aligned}$$

8. Annular loss around drill collars:

$$v_c = \frac{(1.08)(30) + 1.08 \sqrt{(30)^2 + (9.3)(10)(1.125)^2}(10)}{(10)(1.125)}$$

$$= 7.25 \text{ ft/sec}$$

Note: The hydraulically equivalent diameter, d_e , of the annulus

$$7.875 - 6.750 = 1.125 \text{ in}$$

$$\text{The } V_{act} = \frac{308}{(2.45)[(7.875)^2 - (6.75)^2]}$$

$$= 7.6 \text{ ft/sec}$$

\therefore flow is turbulent

and

$$N_{re} = \frac{(2970)(10)(7.6)(1.125)}{30} = 8450$$

$$f = 0.0098, \text{ Curve II}$$

\therefore ,

$$\Delta P_{fac} = \frac{(0.0098)(10)(500)(7.6)^2}{(25.8)(1.125)} = 97 \text{ psi}$$

9. Annular loss around drill pipe

$$v_c = \frac{(1.08)(30) + 1.08 \sqrt{(30)^2 + (9.3)(10)(3.375)^2}(10)}{(10)(3.375)}$$

$$= 4.39 \text{ ft/sec}$$

\therefore , flow is laminar, since circulation volume was calculated from annular velocity of 3 ft/sec;

Use equation

$$\Delta P_{fadp} = \frac{L \gamma_b}{300 d} + \frac{\mu_p v_{act} L}{1500 d^2}$$

$$= \frac{(5500)(10)}{(300)(3.375)} + \frac{(30)(3)(5500)}{1500(3.375)^2}$$

$$= 83 \text{ psi}$$

The total Pressure drop in the system:

$$\Delta P_t = 27 + 270 + 108 + 580 + 97 + 83 \\ \approx 1165 \text{ psi}$$

The horsepower output at the pump is

$$HP = \frac{QP}{1714}$$
$$HP = \frac{(308)(1165)}{1714} = 209$$

The input power from engine to pump (90% pump volumetric efficiency and 85% mechanical efficiency) is:

$$HP = \frac{209}{(0.9)(0.85)} = \underline{\underline{273}}$$