

Key Solution

CHEN 490 – Fundamentals of Petroleum Engineering
HW # 1 – due 1/10/2013

1. Given the analysis in the table below of a natural gas produced from an oil well.

Component	(1) Mol %	(2) M wt.	(3) (1)X(2)	(4) P _c , psia	(5) T _c , R	(6) (1)X(4)	(7) (1)X(5)
Methane	79.05	16.04	12.70	673	344	531	272
Ethane	10.85	30.07	3.26	709	550	77.0	59.7
Propane	4.61	44.09	2.03	618	646	28.5	30.7
Iso-butane	1.28	58.12	0.74	530	530.33	6.8	9.4
n-butane	2.04	58.2	1.19	551	551.36	11.2	15.6
iso-pentane	0.21	72.15	0.15	482	482.36	1.0	1.7
n-pentane	0.34	72.15	0.25	485	485.47	1.6	2.9
hexane	0.84	86.17	0.72	434	434.15	3.6	7.7
heptanes +	0.78	140.0	1.09	405	405.172	3.2	9.2
	100.0		22.13			664 psia	409 R

Compute:

- The gas gravity
 - The pseudo-critical pressure & temperature
 - The compressibility factor, z, (use Standing & Katz chart)
- M wt. C₇₊ = 140
Sp. gravity of C₇₊ = 0.85
- What volume will 100 lb of the above gas occupy at p = 300 psig, T = 170 F?
 - (a) What is the density of a miscellaneous 0.90 gravity gas at 2000 psia and 150 F?
(b) What is the specific volume at these conditions?
 - A cylindrical tank contains miscellaneous 0.8 gravity gas at 2500 psia and 100 F. The volume of the tank is 10 ft³.
 - How many moles of gas in the tank?
 - What standard volume of gas is this?
 - 1000 scf of gas is released from the tank. This causes the temperature to fall to 60 F. What is the final tank pressure?

Solution:

1(a) Column (1) is given. Column (2) is obtained from Table (Physical Properties of Light Paraffins), and the molecular weight of the mixture is the total of column (3).

$$\text{Gas gravity} = G_g = \frac{\text{density of gas at std. cond.}}{\text{density of air at std. cond.}}$$

Since one mole of any gas occupies the same volume at std. conditions (379 ft^3),

$$G_g = \frac{22.13/379}{29/379} = \frac{22.13}{29} = \underline{0.76}$$

where 29 = mol wt of air.

(b) The C_7+ fraction is ^{itself} a mixture, and the Pseudo-Critical properties must be obtained from Figure 1.5 attached. The other values in columns (4) and (5) are ^{from} Table.

$$p_c = \underline{664} \text{ psia}, \quad p_{Tc} = \underline{409} \text{ }^\circ\text{R}$$

$$2 \quad PV = ZnRT$$

$$V = \frac{ZnRT}{P} \quad , \quad n = \frac{m}{M} = \frac{100}{22.1} = 4.52 \text{ moles}$$

To obtain Z from the Chart (Standing & Katz)

$$\text{Reduced pressure, } P_r = \frac{P}{p_c} = \frac{3015}{664} = 4.54$$

$$\text{Reduced temp., } T_r = \frac{T}{p_{Tc}} = \frac{630}{409} = 1.54$$

From this, $Z \cong 0.81$ and

$$V = \frac{(0.81)(4.52)(10.7)(630)}{3015} = \underline{8.2 \text{ ft}^3}$$

3(a) $Z \cong 0.67$ from attached figure ^{0.90} gravity (1.11)
 natural gas; then using eq.

$$\rho = \frac{PM}{ZRT} = \frac{(2000)(29)(0.90)}{(0.67)(10.73)(610)} = \underline{11.9 \text{ lb/ft}^3}$$

$$(b) \quad v = \frac{1}{\rho} = \frac{1}{11.9} = \underline{0.084 \frac{\text{ft}^3}{\text{lb}}}$$

$$4 (a) \quad n = \frac{PV}{ZRT} = \frac{(2500)(10)}{(0.67)(10.7)(560)} = \underline{6.2}$$

$$(b) \quad V_s = (6.2)(379) = \underline{2350 \text{ scf}}$$

or

$$\frac{P_s V_s}{T_s} = \frac{PV}{ZT}$$

$$V_s = \frac{PV}{ZT} \times \frac{T_s}{P_s} = \frac{(2500)(10)(526)}{(0.67)(560)(14.7)} = \underline{2350 \text{ scf}}$$

$$(c) \quad \text{Mol remaining} = 6.2 - \frac{1000}{379} = 3.6 \text{ moles}$$

$$P = \frac{ZnRT}{V}$$

But $Z = \text{function of } P$, \therefore the solution requires trial and error.

$$\frac{P}{Z} = \frac{(3.6)(10.7)(520)}{10} = 2000$$

Assume

1) $P = 1500$, then $Z = 0.581^*$

$$\frac{P}{Z} = 2580 \text{ (high)}$$

2) $P = 1300$, then $Z = 0.617^*$

$$\frac{P}{Z} = 2100 \text{ (high)}$$

(3) $P = 1250$, then $Z = 0.627^*$

$$\frac{P}{Z} = 1955 \approx 2000 \text{ (close enough)}$$

final $P = 1250$ psia

* Values of Z are obtained at 60°F at the assumed pressures from the 0.80 gravity chart (attached).

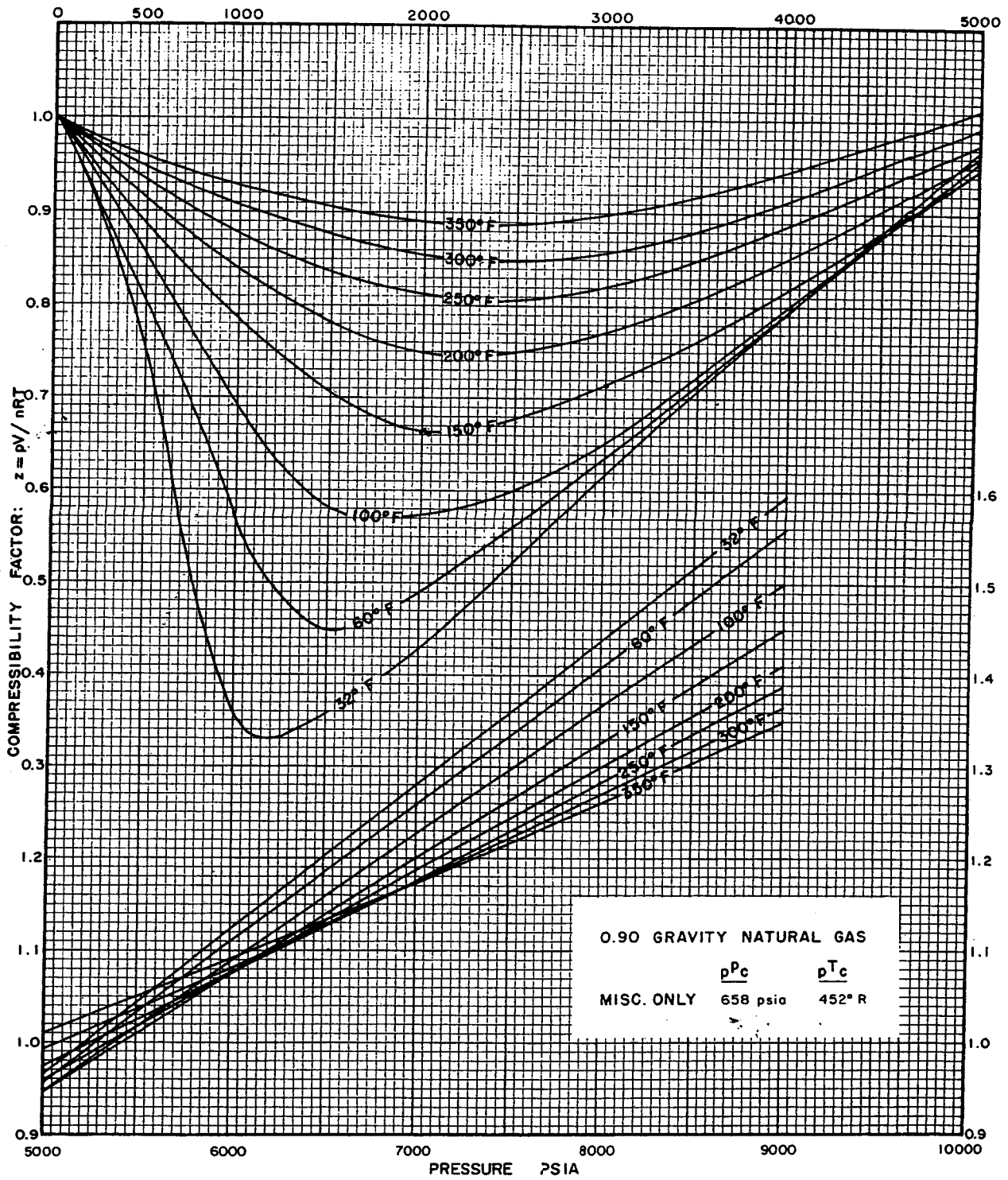


Fig. 1.11. 0.90 gravity natural gas, miscellaneous only.

TABLE 4-4. PHYSICAL CONSTANTS OF HYDROCARBONS
(Values from CNGA and NGAA. Modified for standard conditions of 60°F and 14.65 psia)

	Methane	Ethane	Propane	Iso-butane	Normal butane	Iso-pentane	Normal pentane	Normal hexane	Normal heptane	Heptanes plus C ₇₊
Molecular formula	CH ₄	C ₂ H ₆	C ₃ H ₈	<i>i</i> -C ₄ H ₁₀	<i>n</i> -C ₄ H ₁₀	<i>i</i> -C ₅ H ₁₂	<i>n</i> -C ₅ H ₁₂	<i>n</i> -C ₆ H ₁₄	<i>n</i> -C ₇ H ₁₆	<i>M</i> —
Molecular weight	16.042	30.068	44.094	58.120	58.120	72.146	72.146	86.172	100.198	
Critical temp, °F abs	✓ 343	✓ 550	✓ 666	733	765	830	847	914	972	
Critical pressure, psia	673	708	617	530	551	482	485	434	397	
Critical density, lb/gal	1.351	1.695	1.888	1.945	1.891	1.955	1.935	1.958	1.957	
Critical volume, (cu ft/lb-mole)	1.586	2.371	3.123	3.990	4.130	4.930	4.98	5.88	6.84	
SG gas (air = 1.00)	0.554	1.038	1.522	2.006	2.006	2.491	2.491	2.975	3.459	<i>M</i> /28.966
Cu ft/lb gas	23.73	12.66	8.63	6.55	6.55	5.28	5.28	4.42	3.80	380.69/ <i>M</i>
Cu ft gas/gal of liquid	59.18	39.43	36.56	30.75	31.89	27.50	27.76	24.46	21.77	3170 <i>S</i> / <i>M</i>
Lb Mcf of gas	42.14	78.98	115.83	152.67	152.67	189.51	189.51	226.36	263.20	2.6268 <i>M</i>
Gal liquid per Mcf of gas	16.87	25.36	27.38	32.57	31.41	36.41	36.07	40.94	45.94	0.3155 <i>M</i> / <i>S</i>
Bbl liquid/MMcf of gas	401.6	603.9	651.9	775.4	747.5	867.0	858.8	974.8	1094	7.511 <i>M</i> / <i>S</i>
SG liquid (60/60)	0.3	0.374	0.508	0.563	0.584	0.625	0.631	0.664	0.688	<i>S</i>
Lb/gal liquid at 60°F	2.5	3.11	4.23	4.69	4.86	5.20	5.25	5.53	5.73	8.327 <i>S</i>
Lb/bbl liquid at 60°F	105	130.6	177.7	197.0	204.1	218.4	220.5	232.3	240.7	349.7 <i>S</i>
Lb/cu ft liquid at 60°F	18.70	23.26	31.64	35.08	36.35	38.90	39.27	41.36	42.86	62.29 <i>S</i>
Cu ft liquid/lb at 60°F	0.0535	0.0430	0.0316	0.0285	0.0275	0.0257	0.0254	0.0242	0.0233	0.01605/ <i>S</i>
Gal/lb-mole at 60°F	6.4	9.64	10.41	12.38	11.94	13.84	13.71	15.57	17.47	0.120 <i>M</i> / <i>S</i>

Constants Used in Calculations

1 cu ft = 28.316 liters
1 cu ft = 7.480 gal
1 gal = 3,785.53 ml
760 mm Hg = 14.696 psi

0°F = 459.58°R
Density of water at 60°F = 8.327 lb per gal
Molecular weight of air = 28.966
1 mole = 380.69 cu ft of perfect gas at 14.65 psia and 60°F

**Physical Properties of Light Paraffin
Hydrocarbons and Miscellaneous Components**

Compounds			Critical	Critical
Abbreviation		Molecular	pressure	Temperature
of formula	Name	weight	psia	Rankine
C ₁	Methane	16.04	673	344
C ₂	Ethane	30.07	709	550
C ₃	Propane	44.09	618	666
iC ₄	iso-Butane	58.12	530	733
nC ₄	normal-Butane	58.12	551	766
iC ₅	iso-Pentane	72.15	482	830
nC ₅	n-Pentane	72.15	485	847
nC ₆	n-Hexane	86.17	434	915
nC ₇	n-Heptane	100.2	397	973
nC ₈	n-Octane	114.2	370	1025
nC ₉	n-Nonane	128.3	335	1073
nC ₁₀	n-Decane	142.3	312	1115
-	Air	28.97	547	239
N ₂	Nitrogen	28.02	492	227
O ₂	Oxygen	32.00	732	278
CO ₂	Carbon Dioxide	44.01	1072	548
H ₂ S	Hydrogen Sulfide	34.08	1306	673
H ₂ O	Water	18.02	3206	1165